

4. (Once Amended) The method of claim 1, in which use is made of feedstocks having a sulphur content of not more than 5 %wt.
5. (Once Amended) The method of claim 1, in which a hydrocarbonaceous feedstock is used containing between about 5 %wt and about 40 %wt of material having a boiling point range which is the same as or higher than the boiling point range of the hydroprocessed product to be produced.
6. (Once Amended) The method of claim 5, in which the feedstock contains between about 5 %wt and about 40 %wt of material having a boiling point above the final boiling point of the hydroprocessed product.
7. (Once Amended) The method of claim 1, in which kerosene and/or gas oil are recovered as hydroprocessed product(s) from the hydrotreated feedstock.
8. (Once Amended) The method of claim 1, in which part or all of the non-recovered material from the treatment with hydrogen is subjected to a catalytic oxidation process which produces hydrogen and carbon (di) oxide.
9. (Once Amended) The method of claim 8, in which the catalytic oxidation process comprises a catalytic partial oxidation process.
10. (Once Amended) The method of claim 8, in which hydrogen not used in the hydrotreatment step is used at least partially to produce electricity by feeding it to a fuel cell which is operated to deliver electricity and water (steam).
11. (Once Amended) The method of claim 10, in which the electricity in excess of that needed for the utilities of the process is produced from excess hydrogen.
12. (Once Amended) The method of claim 10, in which at least part of the steam needed in the hydrogen manufacturing unit is provided by the fuel cell.

13. (Once Amended) The method of claim 1, in which kerosene and/or gas oil, are produced from no feedstocks other than the hydrocarbonaceous feedstock and water used in the watergas-shift step.

14. (Once Amended) The method of claim 1, in which hydrogen sulphide generated by the treatment with hydrogen is converted into elemental sulphur by conventional means.

15. (Once Amended) The method of claim 1, in which use is made of a catalyst system capable of converting at least about 50 %wt per pass of the material, having a boiling point range which is the same or above the boiling point range of the hydroprocessed product.

16. (Once Amended) The method of claim 15, in which use is made of a catalyst containing zeolite beta as active component in the treatment with hydrogen.

17. (Once Amended) The method of claim 16, in which the zeolite beta-based catalyst is capable of converting at least 90 %wt per pass of the fraction to be treated to obtain the hydroprocessed product.

18. (Once Amended) The method of claim 15, in which the treatment with hydrogen is carried out at a temperature between about 100°C and about 550 °C.

19. (Once Amended) The method of claim 15, in which the treatment with hydrogen is carried out at a pressure of up to 400 atmospheres.

20. (Once Amended) The method of claim 10, in which the fuel cell step is operated in such a way that it delivers excess electricity.

21. (Once Amended) The method of claim 9, in which the catalytic partial oxidation step and the fuel cell step are operated in such a way that they generated the internal needs on hydrogen and electricity for the process.

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22. (Once Amended) The method of claim 9, in which the hydrogen generated by the catalytic partial oxidation step has been produced at least partly from hydrocarbons containing at most 4 carbon atoms present in the hydrocarbonaceous feedstock or as produced during the hydrotreatment step.

23. (Once Amended) The method of claim 22, in which the feedstock for the catalytic partial oxidation step consists of hydrocarbons having about 4 or less carbon atoms.

24. (Once Amended) The method of claim 1, in which hydrogen is separated off from the hydrotreated feedstock and from the hydroprocessed product if the latter is not to be recovered prior to the hydrogen manufacturing step.

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Add new claims:

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25. The method of claim 1, in which use is made of feedstocks having a sulphur content below 3 %wt.

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26. The method of claim 8, in which the catalytic oxidation process comprises a watergas-shift process.

27. The method of claim 1, in which hydrogen is produced from no feedstocks other than the hydrocarbonaceous feedstock and water used in the watergas-shift step.

28. The method of claim 1, in which carbon dioxide is produced from no feedstocks other than the hydrocarbonaceous feedstock and water used in the watergas-shift step.

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27. The method of claim 1, in which electricity is produced from no feedstocks other than the hydrocarbonaceous feedstock and water used in the watergas-shift step.

Rule 128

~~30~~<sup>28</sup>. The method of claim 1, in which use is made of a catalyst system capable of converting at least about 65 %wt per pass of the material, having a boiling point range which is the same or above the boiling point range of the hydroprocessed product.

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~~31~~<sup>29</sup>. The method of claim 15, in which the treatment with hydrogen is carried out at a temperature between about 250°C and about 450 °C.

~~32~~<sup>30</sup>. The method of claim 15, in which the treatment with hydrogen is carried out at a pressure of between about 10 and 200 atmospheres.

Respectfully submitted,  
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